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On time discretizations for the simulation of the settling-compression process in one dimension

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Abstract

The simulation model for secondary settling tanks by Bürger et al. (2013) was introduced mainly to resolve spatial discretization problems when both hindered settling and the phenomena of compression and dispersion are included. Straightforward time integration unfortunately means long computational times. The next step in the development is to introduce and investigate time-integration methods for more efficient simulations, but where other aspects such as implementation complexity and robustness are equally considered. The key findings are partly a new time-discretization method and partly its comparison with other specially-tailored and standard methods. Several advantages and disadvantages for each method are given. One conclusion is that the new linearly implicit method is easier to implement than another one (semi-implicit method), but less efficient based on two types of batch sedimentation tests.

Keywords: secondary settling tank; clarifier; benchmark simulation; Bürger-Diehl simulation model; efficiency; linearly implicit time integration

Introduction

Benchmark simulations of entire wastewater treatment plants (WWTPs) are today performed with one-dimensional simulation models of the secondary settling tank (Gernaey et al., 2014; Li and Stenstrom, 2014). In the model by Bürger et al. (2011, 2013), sometimes referred to as “Bürger-Diehl model”, the physical phenomena of hindered settling, volumetric bulk flows, compression of the sludge at high concentrations and dispersion of the suspension near the feed inlet can be included in a flexible way. Each phenomenon is associated with a separate constitutive function with its model parameters, and can be activated or de-activated at the user’s discretion. The possibility to include sludge compression is particularly important, since this improves the predictive power considerably (De Clercq, 2008; Ramin et al., 2014; Van Loosdrecht et al., 2015; Torfs et al., 2015;

Guyonvarch et al., 2015). However, the inclusion of physical phenomena that result in second-order derivative terms in the model partial differential equation (PDE), e.g. compression, means that straightforward time-discretization leads to long simulation times.

Bürger et al. (2013) presented implementation details of a numerical algorithm, which gives reliable simulations with respect to the underlying physical principles and can be obtained with a user-defined accuracy. For long-time simulations of entire WWTPs, it is important to keep discretization errors small. This calls for a fine resolution in both space (many layers in the settler) and time (short time steps), which implies long computational times. Conversely, fast computations are obtained with a low resolution in space and time come at the cost of poor accuracy.

In scientific computing, the numerical error is a measure of how close a numerical solution is to the exact solution or reference solution (obtained by a very fine discretization) of the model, i.e., the governing differential equation. The efficiency of a numerical method is assessed by relating the numerical errors to the computational (central processing unit; CPU) times necessary to obtain the numerical solutions for different discretizations. It is then said that one numerical method is more efficient than another if it allows to obtain a numerical solution with a determined numerical error in less CPU time, or equivalently, a given budget of CPU time allows one to obtain a more accurate numerical solution by the first method than by the second.

The simulation model by Bürger et al. (2013) is based on a method-of-lines formulation of the underlying nonlinear PDE. This means a system of time-dependent ordinary differential equations (ODEs), one for each layer of the settler. Simulations of PDEs are stable and reliable if a so-called CFL (Courant-Friedrichs-Lewy) condition is satisfied. This gives a maximal time step Δt for each given layer thickness Δz . If only hindered settling and bulk flows are included, then the CFL condition means that Δt can be chosen proportional to Δz , i.e., $\Delta t \sim \Delta z$, which results in fast simulations. When compression or dispersion is included and standard ODEs solvers used, the CFL condition states that $\Delta t \sim (\Delta z)^2$, which means very small Δt when the error should be reduced (small Δz is chosen).

The purpose of this contribution is to investigate different time-integration methods, of which one is new, with respect to efficiency and other aspects, such as implementation complexity. There is a qualitative difference in the numerical treatment depending on whether only hindered settling and bulk flows are considered or, if in addition, compression or dispersion are included. For clarity of presentation, we limit ourselves here to batch sedimentation in a vessel with a constant cross-sectional area, and for which the depth z is measured from the suspension surface downwards to the bottom at $z = B$. The model partial differential equation (PDE) is

$$\frac{\partial C}{\partial t} = -\frac{\partial f(C)}{\partial z} + \frac{\partial}{\partial z} \left(d(C) \frac{\partial C}{\partial z} \right), \quad 0 < z < B, \quad t > 0, \quad (1)$$

where the flux function $f(C) = C v_{\text{hs}}(C)$ contains the hindered settling velocity function $v_{\text{hs}}(C)$ and the compression function is $d(C) = K v_{\text{hs}}(C) \sigma_e'(C)$, where K is a constant containing the solid and fluid mass densities and the acceleration of gravity, and σ_e is the effective solid stress function, which is zero below a critical concentration and increasing above.

Methods

As hindered settling velocity function we choose for simplicity $v_{\text{hs}}(C) = v_0 e^{-rC}$ with $v_0 = 10$ m/h and $r = 0.45$ m³/kg, and the effective solids stress is chosen such that its derivative satisfies

$$\sigma'_e(C) = \begin{cases} 0 & \text{for } 0 \leq C \leq C_c, \\ \alpha(C - C_c) & \text{for } C > C_c, \end{cases}$$

where $\alpha = 0.5$ m²/s² and $C_c = 6$ kg/m³. To obtain a working numerical method an important preparation is to compute the primitive D of d , which can be obtained exactly with the chosen functions. Otherwise, this can be done numerically (Bürger et al., 2013). Then (1) can be written as

$$\frac{\partial C}{\partial t} = \frac{\partial}{\partial z} \left(-f(C) + \frac{\partial D(C)}{\partial z} \right).$$

For batch sedimentation, this PDE should be complemented with initial data $C(z, 0) = C_0(z)$ and zero-flux boundary conditions

$$-f(C) + \frac{\partial D(C)}{\partial z} \Big|_{z=0} = 0 = -f(C) + \frac{\partial D(C)}{\partial z} \Big|_{z=B}. \quad (2)$$

Suitable numerical schemes for the approximate solution of (1) are based on subdividing the depth interval $[0, B]$ into a number N of layers of equal thickness $\Delta z = B/N$. A discretization in space leads to the following method-of-lines formulation (Bürger et al., 2013), which is a system of N ODEs

$$\frac{dC_1}{dt} = -\frac{G_{3/2}}{\Delta z} + \frac{J_{3/2}}{\Delta z}, \quad (3)$$

$$\frac{dC_j}{dt} = -\frac{G_{j+1/2} - G_{j-1/2}}{\Delta z} + \frac{J_{j+1/2} - J_{j-1/2}}{\Delta z}, \quad j = 2, \dots, N-1, \quad (4)$$

$$\frac{dC_N}{dt} = \frac{G_{N-1/2} - J_{N-1/2}}{\Delta z}, \quad (5)$$

where $C_j(t)$ is the concentration of layer j , $G_{j+1/2}$ denotes the numerical convective flux due to hindered settling between layer j and layer $j+1$, which can be chosen, for instance, as the Godunov flux, and $J_{j+1/2}$ is the compressive numerical flux chosen as

$$J_{j+1/2} = \frac{D(C_{j+1}) - D(C_j)}{\Delta z}.$$

Note that (2) implies that the boundary fluxes $G_{1/2} = J_{1/2} = G_{N+1/2} = J_{N+1/2} = 0$. Implementation details on how to compute these fluxes are provided by Bürger et al. (2013). The last term in (4) now becomes the usual second-order difference approximation of $\partial^2 D(C)/\partial z^2$, i.e.,

$$\frac{J_{j+1/2} - J_{j-1/2}}{\Delta z} = \frac{D(C_{j+1}) - 2D(C_j) + D(C_{j-1}))}{\Delta z^2}. \quad (6)$$

The method-of-lines formulation (3)–(5) is converted into a fully discrete scheme by time discretization. Although a variety of methods could be used for (3)–(5), there is nothing to gain by applying a

standard ODE solver of higher formal order of accuracy than one, e.g. a Runge-Kutta method. On the contrary, this will only cause longer computational times producing the same error as explicit Euler time stepping (Diehl et al., 2015).

For the discussion of the various time-stepping methods, which will take the numerical solution from $t = t_n$ to $t_{n+1} = t_n + \Delta t$, it will be important to carefully distinguish between numerical fluxes and concentrations that are evaluated at the old time step t_n and those evaluated at t_{n+1} , which we mark by the respective upper index n and $n+1$. The time-integration methods compared herein are the following, where k_1, k_2 are constants that depend on the choice of the functions f and d .

The explicit Euler method

The explicit Euler method is used for all simulations in Bürger et al. (2011, 2013). The CFL condition of the fully discrete scheme can be captured by $\Delta t \leq k_2 \Delta z^2$ when Δz is small. The method is easy to implement since all terms in the right-hand side of (3)–(5) are evaluated at $t = t_n$ and therefore each concentration C_j^{n+1} is an explicit function of the known ones at the previous time t_n . Thus, the fully discrete version of (4) is

$$\frac{C_j^{n+1} - C_j^n}{\Delta t} = -\frac{G_{j+1/2}^n - G_{j-1/2}^n}{\Delta z} + \frac{D(C_{j+1}^n) - 2D(C_j^n) + D(C_{j-1}^n)}{\Delta z^2}, \quad j = 2, \dots, N-1,$$

with analogous formulas replacing the boundary updates (3) and (5).

The semi-implicit (SI) method

The SI method (Bürger et al., 2006) is described in detail by Diehl et al. (2015). The CFL condition is $\Delta t \leq k_1 \Delta z$. To advance the solution from t_n to t_{n+1} we must solve the following nonlinear system of algebraic equations, where C_j^{n+1} , $j = 1, \dots, N$, are the unknowns:

$$\frac{C_j^{n+1} - C_j^n}{\Delta t} = -\frac{G_{j+1/2}^n - G_{j-1/2}^n}{\Delta z} + \frac{D(C_{j+1}^{n+1}) - 2D(C_j^{n+1}) + D(C_{j-1}^{n+1})}{\Delta z^2}, \quad j = 2, \dots, N-1, \quad (7)$$

supplemented with analogous formulas replacing the boundary updates (3) and (5). These equations are solved iteratively, for example, by the Newton-Raphson method.

The linearly implicit (LI) method

The idea of the LI method goes back to Berger et al. (1979) and is based on first considering the contribution from the compressive flux term (6) from time t_n to t_{n+1} . The purpose of the LI method is to avoid the numerical solution of the nonlinear system of equations (7). The nonlinearities in (7) are found in the evaluations of the function D . The idea is to replace $D(C_j^n)$ in (7) by ξq_j^n (where ξ is a parameter connected to the convergence of the method) so that

$$\frac{C_j^{n+1} - C_j^n}{\Delta t} = -\frac{G_{j+1/2}^n - G_{j-1/2}^n}{\Delta z} + \xi \frac{q_{j-1}^{n+1} - 2q_j^{n+1} + q_{j+1}^{n+1}}{\Delta z^2}, \quad (8)$$

and to find a simple update formula for q_j^n , $j = 1, \dots, N$, to be executed first in each time step. A stable implicit Euler time step implies the formula

$$\frac{q_j^{n+1} - q_j^n}{\Delta t} = \xi \frac{q_{j-1}^{n+1} - 2q_j^{n+1} + q_{j+1}^{n+1}}{\Delta z^2}.$$

This means that a linear system of equations should be solved for q_j^{n+1} at the next time step. Then (8) can be updated explicitly to obtain C_j^{n+1} .

To completely describe the LI method, we define

$$\xi := \gamma \max_{0 \leq C \leq C_{\max}} d(C),$$

where C_{\max} is a (nominal) maximum concentration and $\gamma > 1$ a parameter. To advance the solution from t_n to t_{n+1} , one proceeds as follows:

1. For $j = 1, \dots, N$, set $q_j^n = D(C_j^n)/\xi$.
2. Solve the following linear system for $q_1^{n+1}, \dots, q_N^{n+1}$:

$$\begin{aligned} \frac{q_1^{n+1} - q_1^n}{\Delta t} &= -\xi \frac{q_1^{n+1} - q_2^{n+1}}{\Delta z}, \\ \frac{q_j^{n+1} - q_j^n}{\Delta t} &= \xi \frac{q_{j-1}^{n+1} - 2q_j^{n+1} + q_{j+1}^{n+1}}{\Delta z^2}, \quad j = 2, \dots, N-1, \\ \frac{q_N^{n+1} - q_N^n}{\Delta t} &= \xi \frac{q_{N-1}^{n+1} - q_N^{n+1}}{\Delta z}. \end{aligned} \tag{9}$$

3. Calculate $C_1^{n+1}, \dots, C_N^{n+1}$ from

$$\begin{aligned} \frac{C_1^{n+1} - C_1^n}{\Delta t} &= -\frac{G_{3/2}^n}{\Delta z} + \frac{q_1^{n+1} - q_1^n}{\Delta t}, \\ \frac{C_j^{n+1} - C_j^n}{\Delta t} &= -\frac{G_{j+1/2}^n - G_{j-1/2}^n}{\Delta z} + \frac{q_j^{n+1} - q_j^n}{\Delta t}, \quad j = 2, \dots, N-1, \\ \frac{C_N^{n+1} - C_N^n}{\Delta t} &= \frac{G_{N-1/2}^n}{\Delta z} + \frac{q_N^{n+1} - q_N^n}{\Delta t}. \end{aligned}$$

Note that the linear system (9) can be written as follows, where $\mu := \Delta t/\Delta z^2$:

$$\begin{bmatrix} 1 + \xi\mu & -\xi\mu & 0 & \dots & 0 \\ -\xi\mu & 1 + 2\xi\mu & -\xi\mu & \ddots & \vdots \\ 0 & \ddots & \ddots & \ddots & 0 \\ \vdots & \ddots & -\xi\mu & 1 + 2\xi\mu & -\xi\mu \\ 0 & \dots & 0 & -\xi\mu & 1 + \xi\mu \end{bmatrix} \begin{pmatrix} q_1^{n+1} \\ \vdots \\ q_N^{n+1} \end{pmatrix} = \begin{pmatrix} q_1^n \\ \vdots \\ q_N^n \end{pmatrix},$$

This tridiagonal linear system of equations can easily be solved, for example by the Thomas algorithm (cf., e.g., Diehl et al., 2015). A preliminary analysis on the stability of the scheme (not presented here) implies that the CFL condition of the LI scheme is

$$\Delta t \leq \frac{\Delta z}{2 \max_{0 \leq C \leq C_{\max}} f'(C)} \left(1 - \frac{1}{\gamma}\right). \tag{10}$$

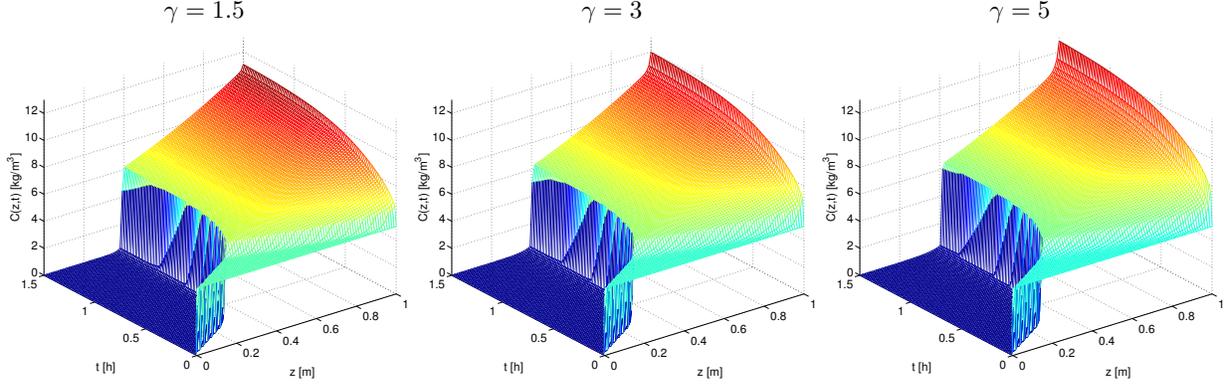


Figure 1: Kynch test simulated by the LI method with $N = 90$ layers and the indicated values of γ .

Other time-stepping methods

Any ODE solver could be used for the method-of-lines system (3)–(5). Possibly competitive methods are adaptive step-size methods and we choose here the ODE solver `ode15s` in Matlab (2014), which is an implicit multi-step method of variable order with step-size control. Of several standard ODE solvers investigated by Diehl et al. (2015) this was the second most efficient one (after the SI method) in the investigations with both stand-alone settler simulations and benchmark simulations for the entire activated sludge process.

Numerical tests

The investigated methods are used for the simulation of two different batch settling tests in a vessel with $B = 1$ m. We consider a conventional Kynch test (KT; Kynch, 1952), that is, the settling of an initially homogeneous suspension, and a Diehl test (DT; Diehl, 2007), where a body of concentrated suspension is initially located above clear liquid, separated by, e.g., a membrane. Both tests provide complementary information that can be used to identify large portions of the flux function f (Betancourt et al., 2014). For both tests we measure the performance of the numerical methods in terms of numerical error and CPU time. The error of a total simulated solution $C_{\text{tot},N}$ with N layers up to a time T is calculated by comparing with a reference solution C_{ref} obtained by Euler’s method and $N = 2430$ layers ($\Delta z = B/N = 1 \text{ m}/2430 \approx 0.41 \text{ mm}$). The relative L^1 error is calculated as

$$E_N = \int_0^T \int_0^B |C_{\text{tot},N}(z, t) - C_{\text{ref}}(z, t)| dz dt \Big/ \int_0^T \int_0^B C_{\text{ref}}(z, t) dz dt .$$

For the KT we choose an initial concentration of $C_0 = 5 \text{ kg/m}^3$ and $T = 1.5 \text{ h}$, which means that almost steady state has been reached. This test is also used to study the dependence of the numerical solutions produced by the LI method on the choice of the parameter γ . For each run, the time step Δt is chosen according to the CFL condition (10) (with equality). Note that the right-hand side of (10) is a decreasing function of γ and it tends to infinity as γ approaches one from above. Figure 1 shows numerical solutions obtained for three different values of γ . This figure and

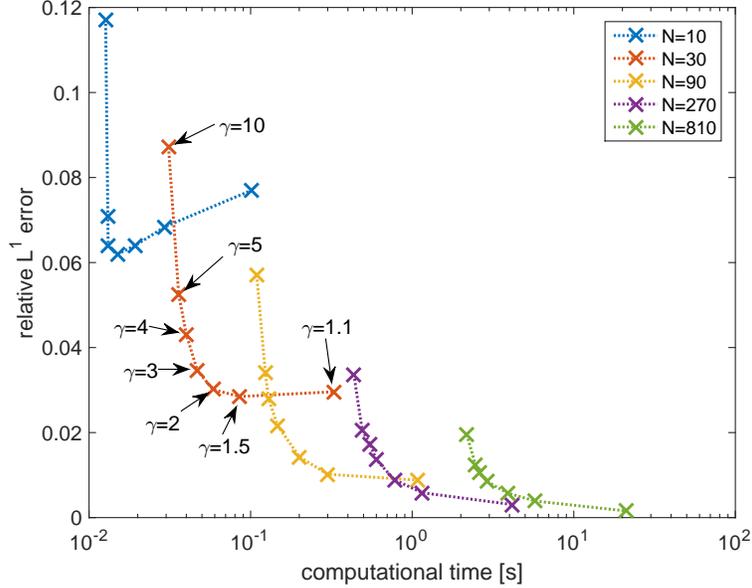


Figure 2: LI method applied to KT: efficiency plots (relative L^1 error versus CPU time) for the indicated values of N , determined for $\gamma = 10, 5, 4, 3, 2, 1.5, 1.1$ (from top to bottom, the curve for $N = 30$ is labeled for illustration).

Figure 2 indicate that for a given number of layers $N > 30$, the values of γ closest to one produce the solutions with the smallest errors, but the highest CPU times. We note that, for instance, for a given value of N the time step for $\gamma = 3$ can be chosen twice larger than that for $\gamma = 1.5$, so the total CPU time for $\gamma = 3$ should be about half of that for $\gamma = 1.5$. Consequently, the choice of γ is subject to the competing goals of accuracy (small errors) and speed (short CPU times) of the simulation. To assess which value of γ is optimal, an efficiency plot (of relative L^1 error versus CPU time) is helpful, see Figure 2. The curves are roughly L-shaped, indicating that γ should be chosen close to the point corresponding to the point of “bend”, since smaller or larger values would lead to larger numerical errors (at only slightly smaller CPU times) or to smaller numerical errors at much increased CPU times. Based on these considerations, the choice $\gamma = 3$ seems a good compromise for further comparison with other methods.

For the Diehl test (DT) we choose the initial data

$$C(z, 0) = \begin{cases} 10 \text{ kg/m}^3 & \text{for } 0 < z < 0.4 \text{ m,} \\ 0 & \text{for } 0.4 \text{ m} < z < B = 1 \text{ m.} \end{cases}$$

Figure 3 shows the numerical solution by the LI method with $\gamma = 3$ and a contour plot of the reference solution. The right plot illustrates that in those regions where $C < C_c$, therefore $d = 0$, and (1) reduces to a first-order hyperbolic PDE, iso-concentration curves are straight lines, in complete agreement with the corresponding theory.

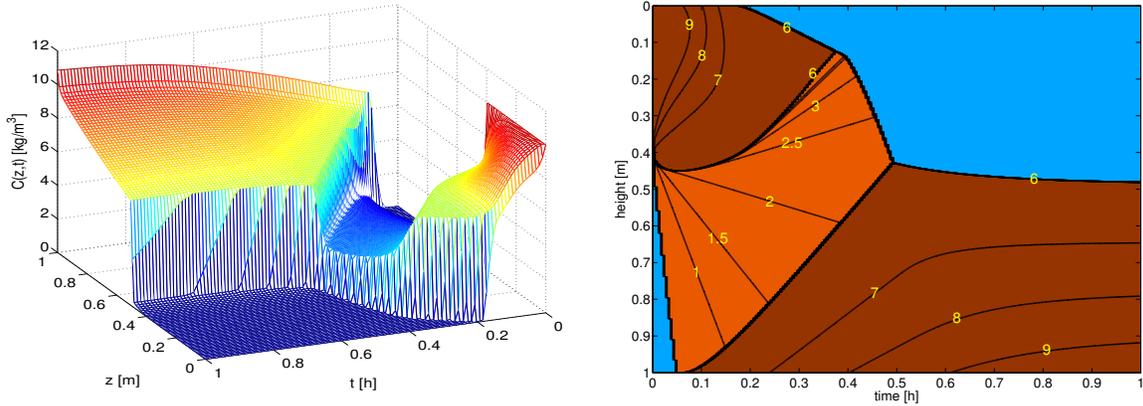


Figure 3: Numerical solution of the DT. Left: solution by the LI method with $\gamma = 3$ and $N = 90$. Right: contour plot of the reference solution, showing areas of $C = 0$ (blue), $0 < C < C_c$ (light brown) and $C > C_c$ (dark brown) and iso-concentration lines corresponding to the annotated values of C [kg/m^3].

Results and discussion

Figure 4 shows the efficiency curves for all methods investigated plus those produced by employing Matlab's `ode15s` solver. It turns out that the latter method is the least efficient, and that for both tests the implicit methods are most efficient, as expected from the corresponding CFL conditions. Moreover, for a given number of layers N , the LI method is the fastest, although not necessarily the one with the smallest error. Note that the efficiency curve for the SI method for the Diehl test (the right plot of Figure 3) is composed of four symbols only. In fact, no information is available for the run with $N = 810$ since the Newton-Raphson iterations did not converge for that case. While this situation could be easily overcome by the ad-hoc remedy of further reducing Δt (say, to 80% of its maximal value determined by the CFL condition), it alerts to a more fundamental problem observed with the SI method; namely that the convergence of (iterative) solvers for the nonlinear equations is not ensured a priori.

For accurate simulation results, Δz should be chosen small, wherefore the CFL condition implies that the explicit Euler method requires much smaller time steps than the other methods. On the other hand, the SI method needs more computations at every time step and requires the evaluation of the Jacobian matrix of the nonlinear algebraic system of equations. However, even when this system is solved by the Newton-Raphson method, the SI method has turned out to be far more efficient than explicit Euler (Diehl et al., 2015). To reduce the implementation complexity and to remove the necessity to solve numerically a system of nonlinear algebraic equations at every iteration in the SI method, whose convergence depends on the Newton-Raphson iterations, the LI method can be used instead. The advantage of solving a linear system only in each iteration, which also means an easier implementation, is paid by the price of a larger numerical error.

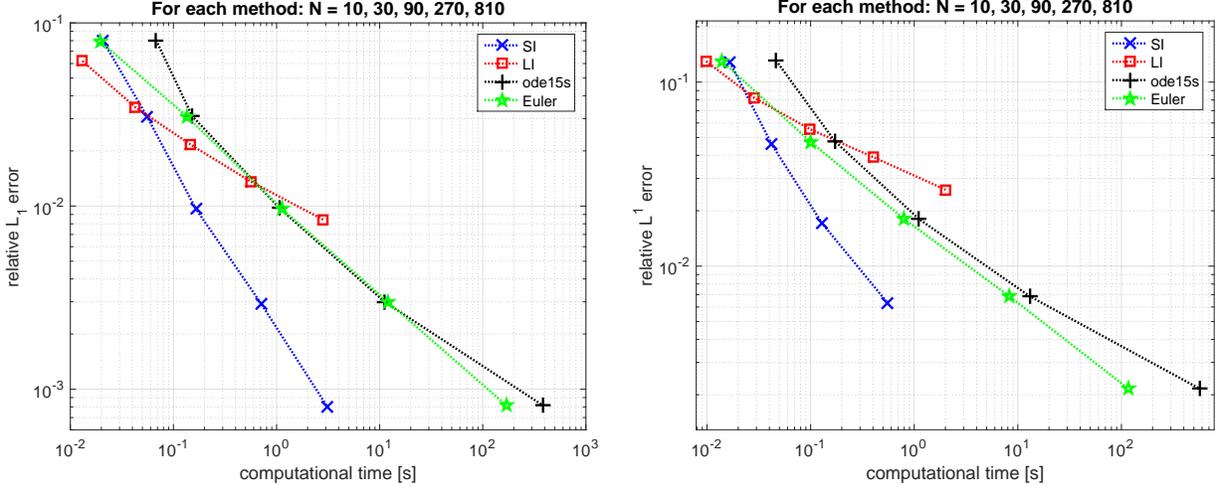


Figure 4: Efficiency plots for the KT (left) and the DT (right) and the Euler, SI and LI methods ($\gamma = 3$) and Matlab’s `ode15s` solver. In the right plot the cross corresponding to $N = 810$ for the SI method is not shown since the Newton-Raphson iterations did not converge, i.e., the method failed.

Conclusions

With the aim of finding an efficient time-integration method for the simulation of sedimentation with compression, we have in this work confined to two batch sedimentation tests for the comparison of some methods. The ideas of the new LI method and its implementation have been provided. When evaluated on the batch settling tests, the following advantages (+) and disadvantages (–) can be concluded:

- Explicit Euler method:
 - + Implementation easy.
 - + Convergence proof exists also for continuous sedimentation (numerical approximate solutions converge to the PDE solution as $\Delta z \rightarrow 0$) by Bürger et al. (2005). Robust method.
 - Not efficient.
- Semi-implicit (SI) method:
 - + Most efficient of the investigated methods. Under the assumption that the Newton-Raphson iterations find a solution each time step, convergence of the numerical method was proved for batch sedimentation by Bürger et al. (2006).
 - Implementation more complex than Euler and LI. At each time step, a nonlinear system of algebraic equations is solved e.g. by Newton-Raphson iterations, which require tolerance parameter to be set. There is no guarantee that these iterations converge.
- Linear-implicit (LI) method:

- + Implementation easy. The ingredient in addition to the Euler method is basically that a linear system of equations is solved at each time step. Robust method.
- ± Second most efficient for $N \approx 100$ for batch sedimentation. The efficiency can be adjusted to some extent by a parameter. Fastest method for a given $N \geq 30$, but least accurate. Convergence proof in preparation.
- Matlab's `ode15s`:
 - + Ready-to-use standard time solver.
 - Implementation most complex of the investigated methods. Well-established robust ODE solver for stiff problems, but not developed for solutions containing discontinuities.
 - Least efficient of the investigated methods.

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